

Fate of 2-Chloro Ethyl Ethyl Sulfide on 13X Molecular Sieve Adsorbent Implications for Regenerative Filtration

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Introduction

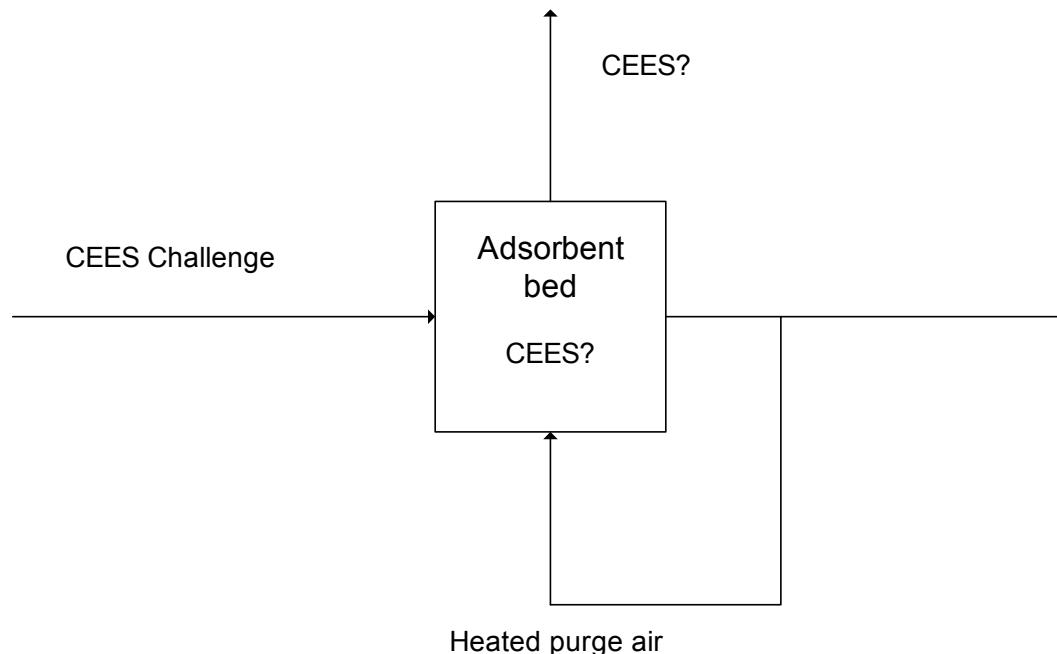
- Regenerative filtration technology offers the promise of greater capacity and breadth of chemical protection than the currently fielded single pass filtration technology.
- Many past and current regenerative filtration prototypes utilize zeolite adsorbents such as 13X molecular sieve.
- The current carbon based adsorbent knowledge base must be expanded to include adsorbate-adsorbent interaction under regenerative filtration conditions.



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Objective

- Evaluate the behavior of 2-chloro ethyl ethyl sulfide (CEES), a mustard (HD) simulant, on 13X molecular sieve under thermal regeneration conditions.





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Approach

- Expose a packed bed of 13X to a vapor challenge of CEES until it reaches saturation.
- Purge the saturated bed with reverse flow and introduce step-wise heating.
- Evaluate at conditions relevant to regenerative filtration.
 - Examine effect of preloaded water.
 - High face velocity (several times that of M48).
 - Restrained adsorbent bed.

Experimental

Preparation of 13X adsorbent

CEES feed concentration	200 mg/m ³ (43 ppm)
Temperature	50 C
Bed depth	3 cm
Flow rate	50 LPM (21.1 C, 1 atm)
Face velocity	51.8 cm/s
Dew point	<-80 C to 0 C

Experimental

Purge of 13X adsorbent

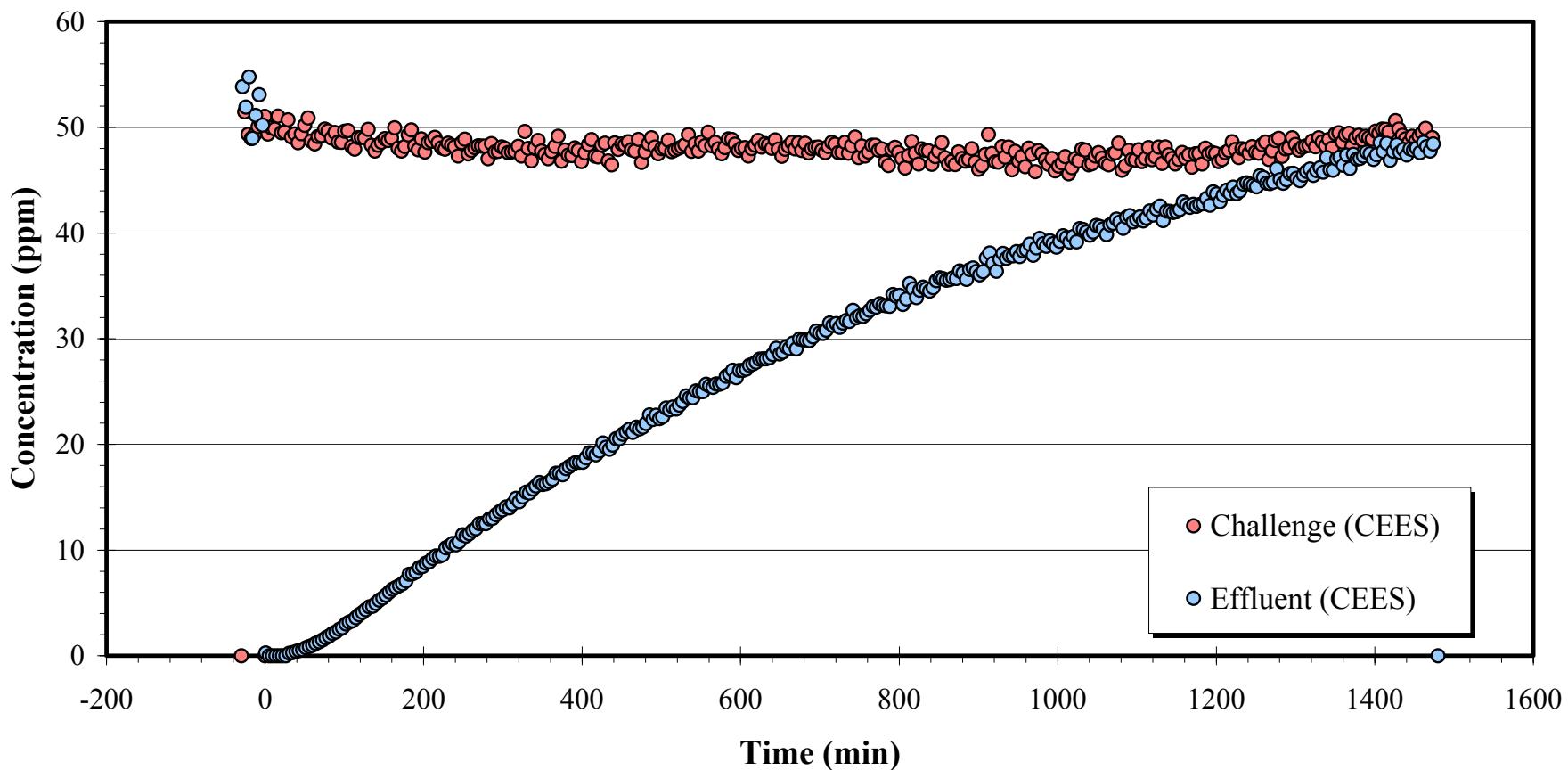
Temperature	50 C to 125 C
Bed depth	3 cm
Flow rate	25 LPM (21.1 C, 1 atm)
Face velocity	25.8 cm/s @ 50 C
Dew point	<-80 C



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Results

Breakthrough of CEES on 13X Adsorbent
43 ppm CEES challenge, 51.8 cm/s velocity, 3 cm bed depth, <-80 C dew point

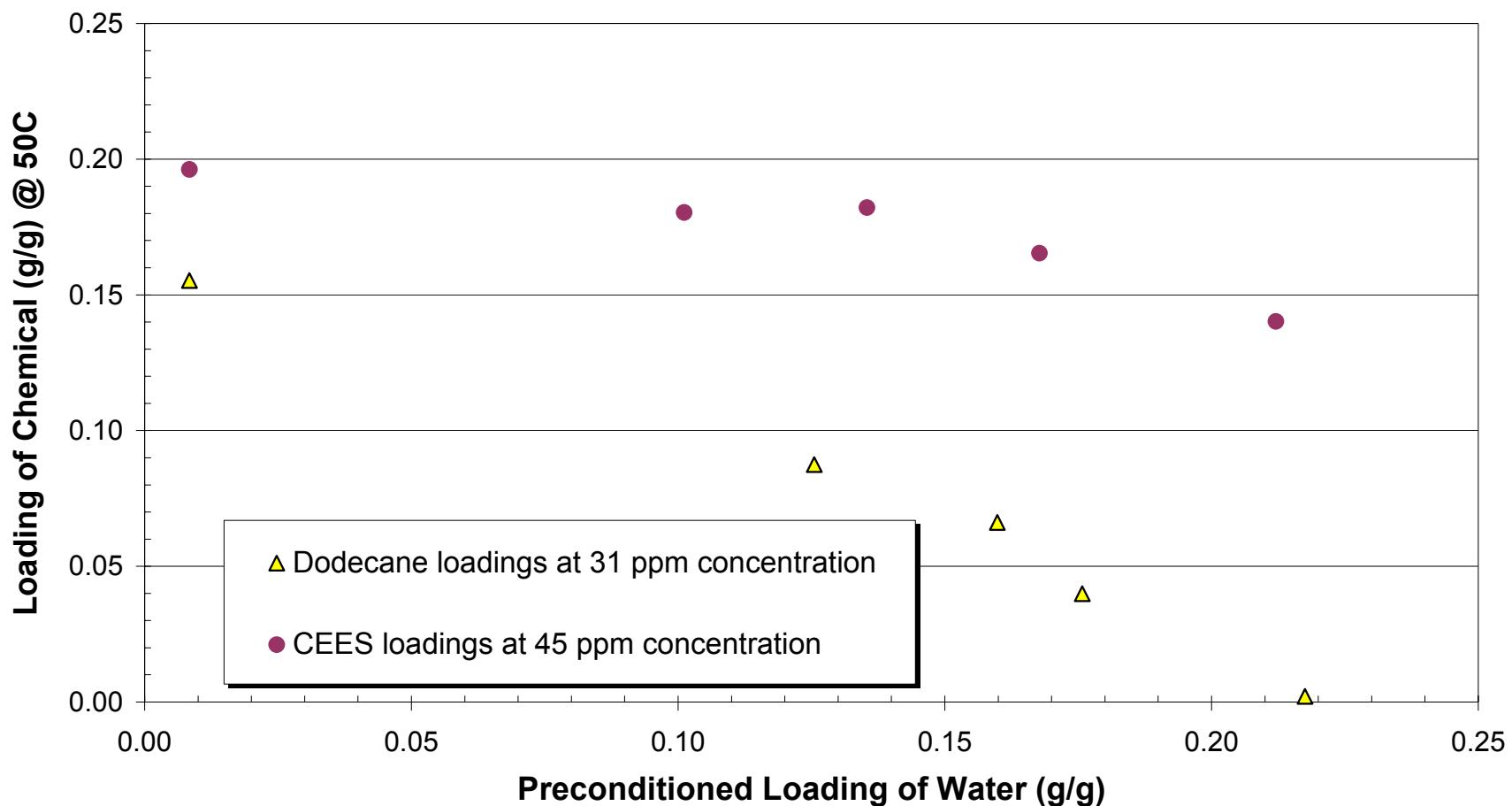




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Results

Chemical Loading From Single Pass Breakthroughs on 13X with Preloaded Water





Results

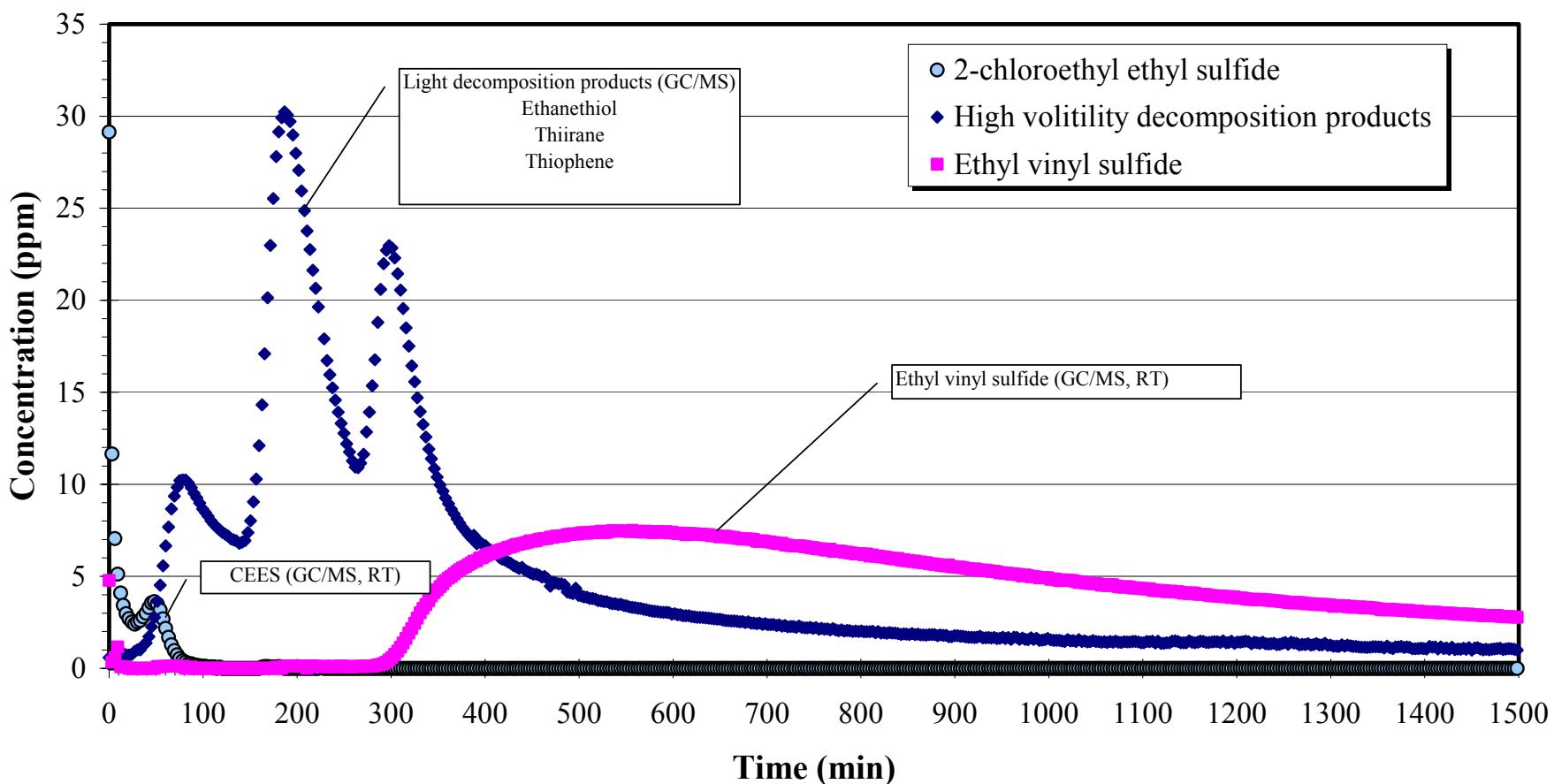
- Identification of purge components
 - Sample 1
 - GC FID
 - One low retention time peak, no other detectable peaks
 - GC/MS suggests presence of following compounds
 - Ethanethiol
 - Thiiirane
 - Thiophene
 - Diethyl sulfide
 - Diethyl disulfide (oxidation product of ethanethiol)
 - CEES
 - Sample 2
 - GC FID
 - CEES peak and two unidentified peaks
 - GC/MS suggests presence of following compounds
 - Ethyl vinyl sulfide
 - CEES
 - Confirmed presence of ethyl vinyl sulfide by matching retention time and response with standard.



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Results

Regeneration of saturated 13X adsorbent
Temperature Programmed Desorption 50 to 125 C

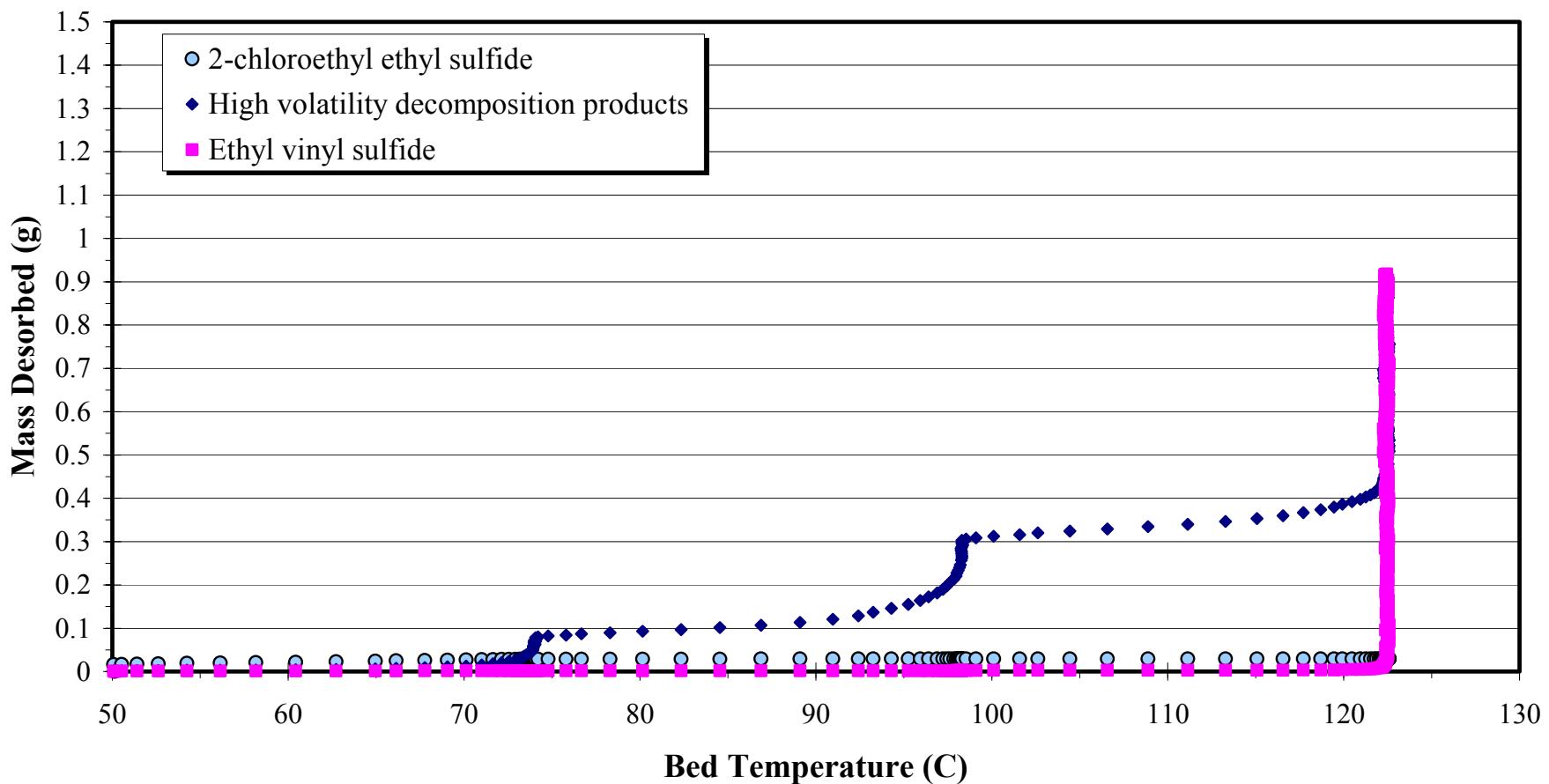




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Results

Regeneration of saturated 13X Adsorbent
Temperature Programmed Desorption 50 C to 125 C
Cumulative Desorbed Mass





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Results

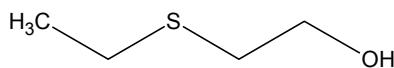
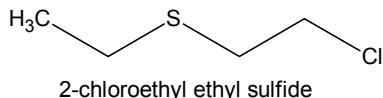
Mass balance

Dew Point	Mass loaded (g)	CEES recovered (g)	Reaction products (g)	Total recovery (%)	Mass balance (%)
< -80 C	7.40	0.04	2.59	36	99
-40 C	6.81	0.06	2.01	31	100
-20 C	6.24	0.03	2.37	38	101

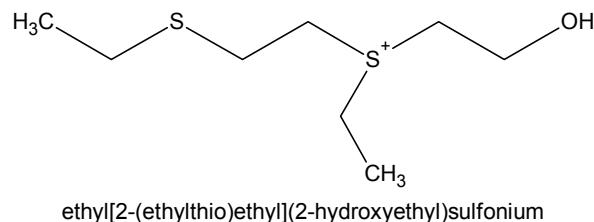
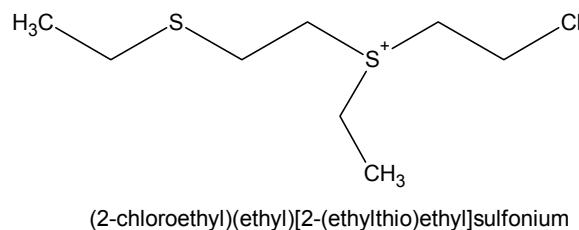


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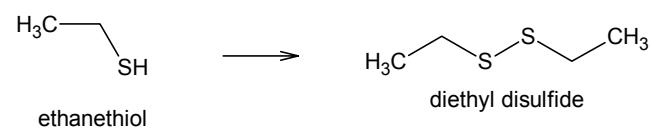
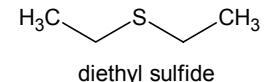
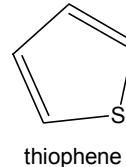
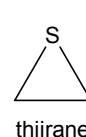
Results



HCl H₂O

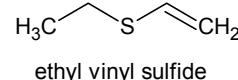


CEES and potential hydrolysis products



Maximum generation 95-120 C

Maximum generation 122 C



Decomposition products



Summary

- One decomposition product identified: ethyl vinyl sulfide.
 - Requires a 122 C bed temperature for desorption.
 - Purges at long times with first order kinetics.
- Several other possible desorption products suggested by data.
 - GC FID method does not allow resolution of 0.64 min RT peak.
 - Possible products are fragments or cyclic derivatives of CEES.
 - Temperature at which the desorption concentration peaks, rises with increased preloaded water (95-120 C).
 - Purges at long times with second order kinetics.



Conclusions

- CEES undergoes hydrolysis and decomposition under conditions relevant to regenerative filtration on 13X adsorbent.
- Less than 1% of loaded CEES is purged as CEES, which is <2% of the total purge mass.
- 13X adsorbent is not fully regenerated when tested with CEES under the test conditions (<50%).
- Future work
 - Test mustard under similar conditions.
 - Literature suggests mustard may be less reactive but produce analogous (mustard chemistry) decomposition products.
 - Design apparatus for screening desorption properties (reactivity, dynamics, equilibrium) for regenerative filtration adsorbent candidates under a wide variety of conditions. This would be an important engineering tool for regenerative filtration system design.



ECBC Acknowledgements

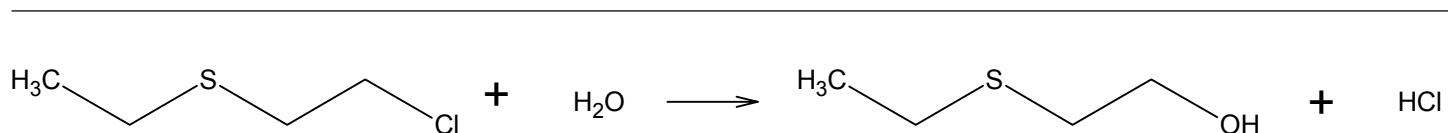
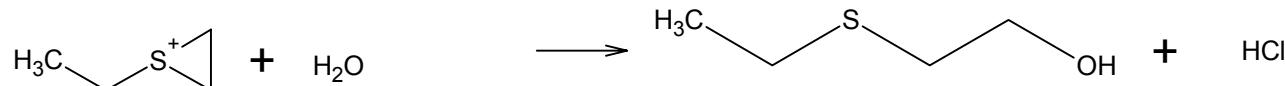
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Background

- Hydrolysis of 2-chloroethyl ethyl sulfide in solution*



- First order kinetics dominate when CEES is infinitely dilute.
- Major hydrolysis products are HEES and HCl.

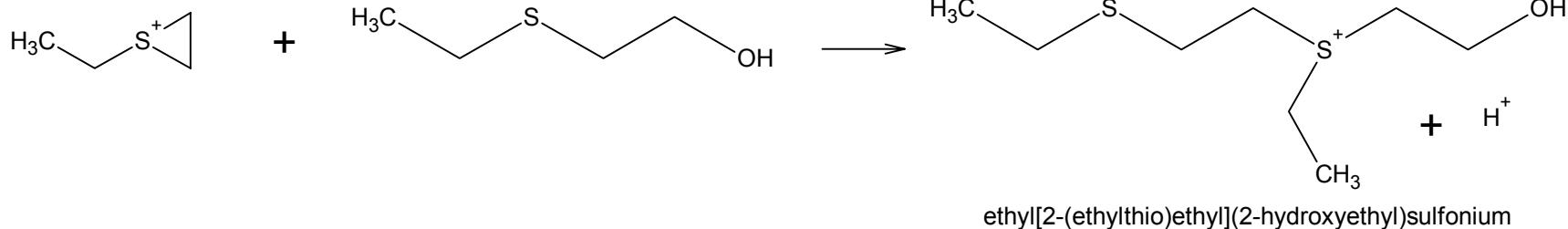
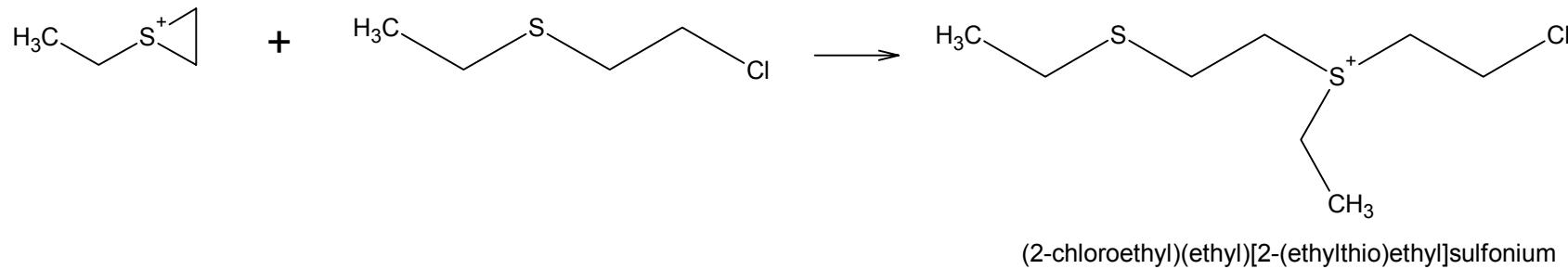
* Yang, Y., et al., "Mechanisms of Interactions of 2-chloroethyl sulfides with Water.", CRDEC-SP-88013, Nov 1987



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Background

- Hydrolysis of 2-chloroethyl ethyl sulfide in solution.
 - For higher concentrations of CEES, reaction proceeds to equilibrium of CEES, HEES, and EHT.

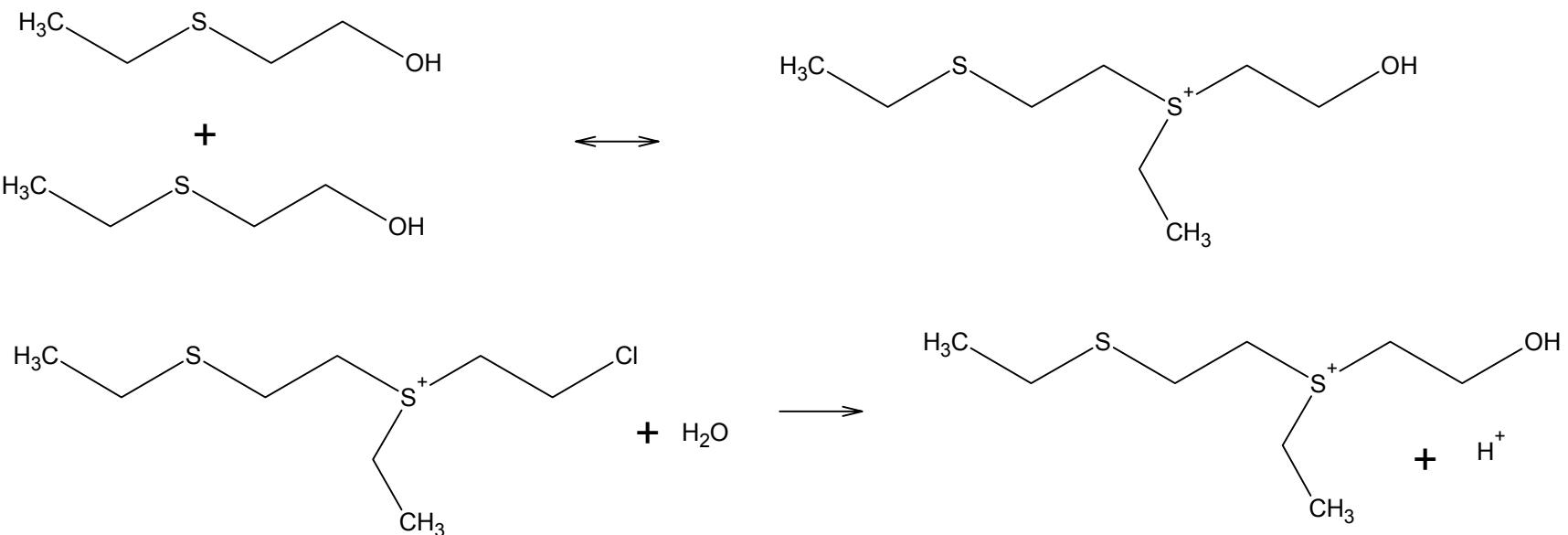




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Background

- Hydrolysis of 2-chloroethyl ethyl sulfide in solution.
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Background

	CEES $\text{CH}_3\text{CH}_2\text{SCH}_2\text{CH}_2\text{Cl}$	Mustard $\text{S}(\text{CH}_2\text{CH}_2\text{Cl})_2$
Molecular weight	124.6	159.1
Boiling point	157.1 C	227.8 C
Specific gravity	1.07 @ 25 C	1.27 @ 20 C
Water solubility*	$4.85 * 10^{-2}$ M	$4.44 * 10^{-3}$ M
Hydrolysis products	HCl, HEES, EHT, sulfonium salts	HCl, CH, TG, sulfonium salts

* Yang, Y. et al., "Solubility Properties and Rates of Solution of Mustard Gas and 2-Chloroethyl ethyl sulfide", CRDEC-TR-88043, February 1988



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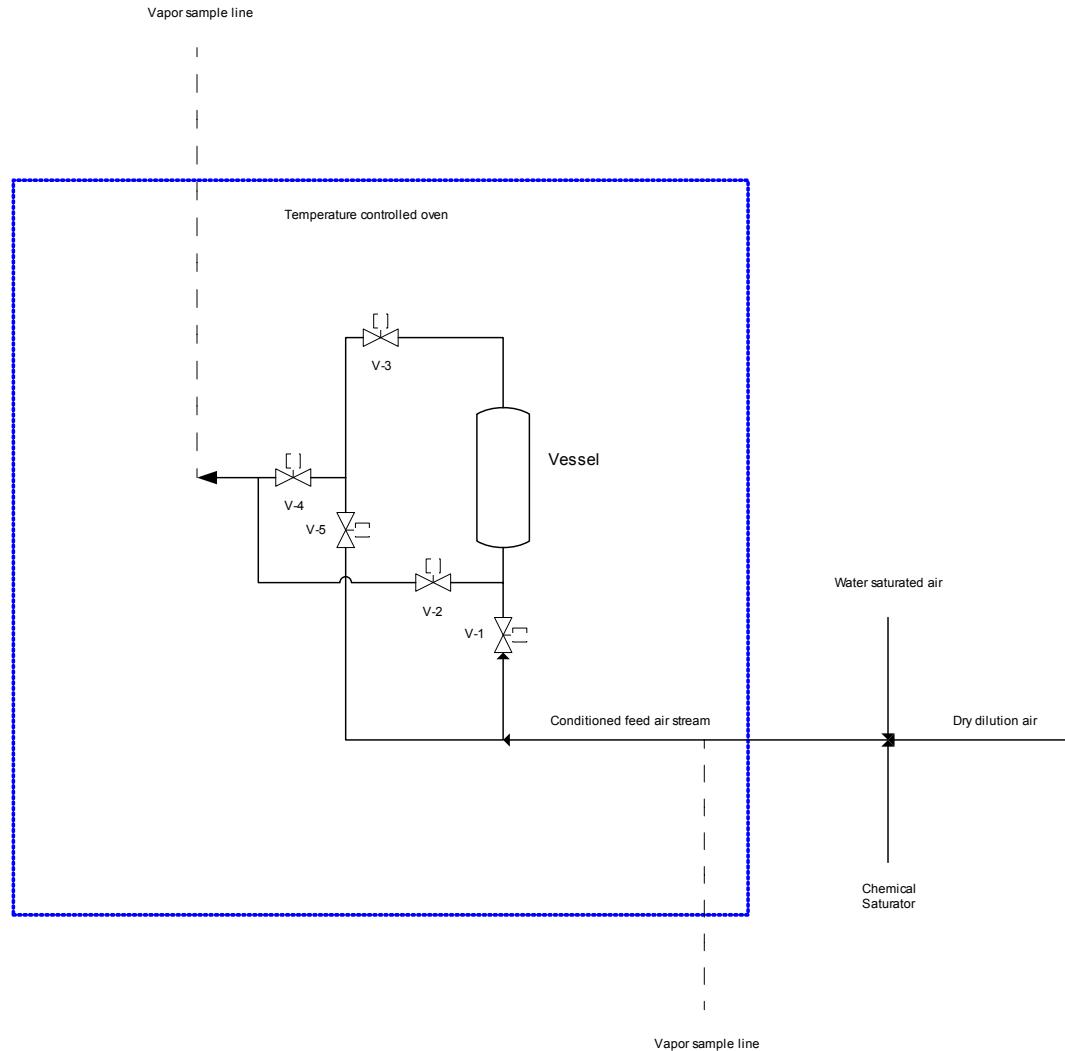
Background

- Behavior of neat HD on NaY (13X)* [room temp]
 - $\text{HD} + \text{H}_2\text{O} \rightarrow \text{CH} + \text{TG} \rightarrow \text{CH-TG}$
- Thermal desorption of HD from CSC carbon**
 - Combination of hydrolysis and thermal decomposition
 - Decomposition products 1,2 dichloroethane, 2-chloroethanol, 1,4 thioxane, 1,4 dithiane, sulfides, ethers
 - Only low level concentrations examined.

* Wagner, G.W., Bartram, P. W., "Reactions of VX, HD, and Their Simulants with NaY and AgY Zeolites. Desulfurization of VX on AgY.", Langmuir. 1999, 15, 8113-8118

** Karwacki, C. J., et al., "Effect of Temperature on the Desorption and Decomposition of HD from Activated Carbon.", ERDEC-TR-555, Dec 1998.

Experimental



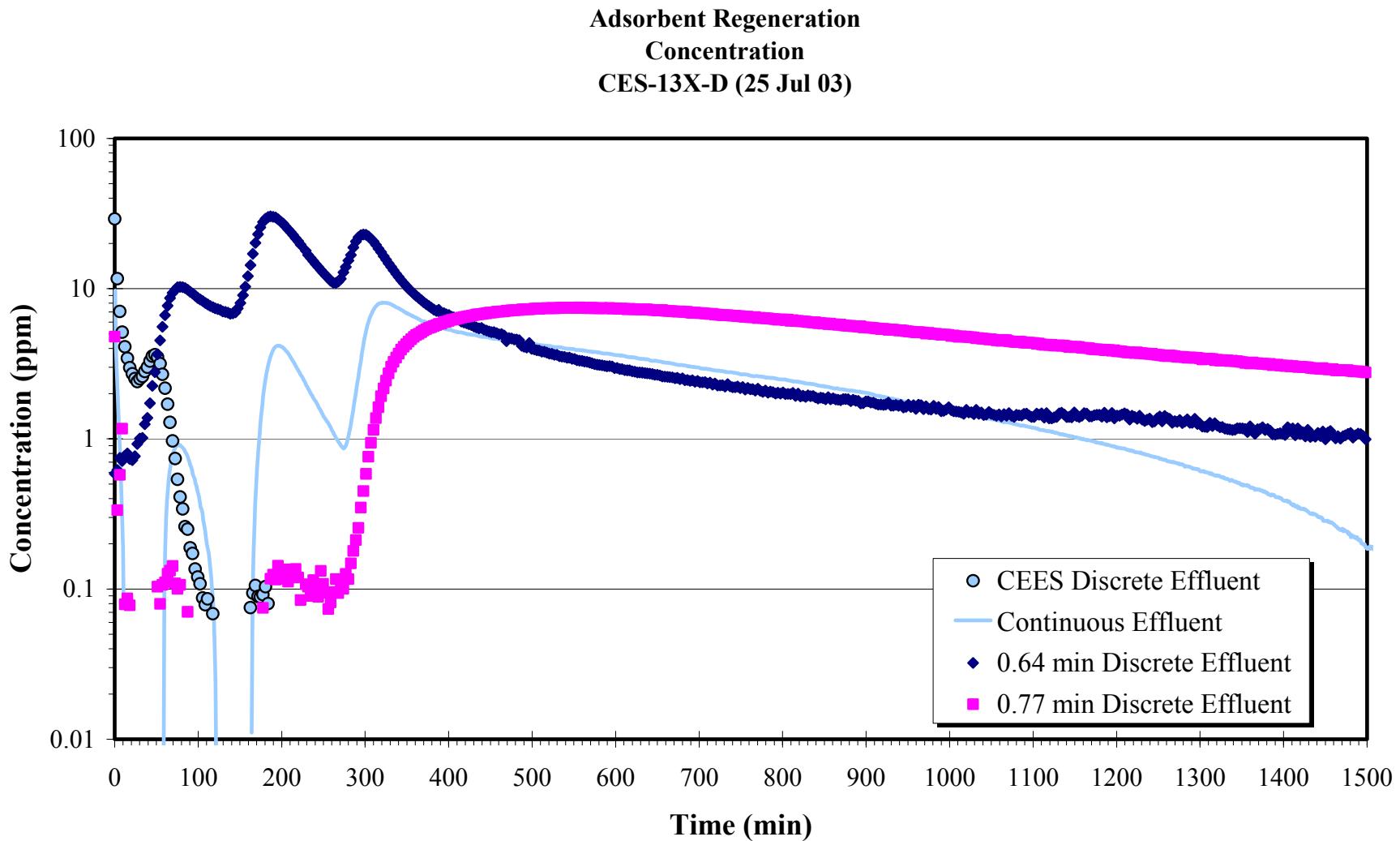
Experimental

- Analytical equipment.
 - Preparation and purge of adsorbent bed.
 - Continuous feed and effluent signal.
 - Direct FID voltage output.
 - Discrete feed and effluent signal.
 - GC fid, 110 c.
 - HP-1701 column (14%-cyanopropyl-phenyl)-methylpolysiloxane).
 - Sampling of bagged purge effluent.
 - Transfer at 25 C at 500 ml/min on Tenax.
 - Desorb contents to GC/MS with FID detector.



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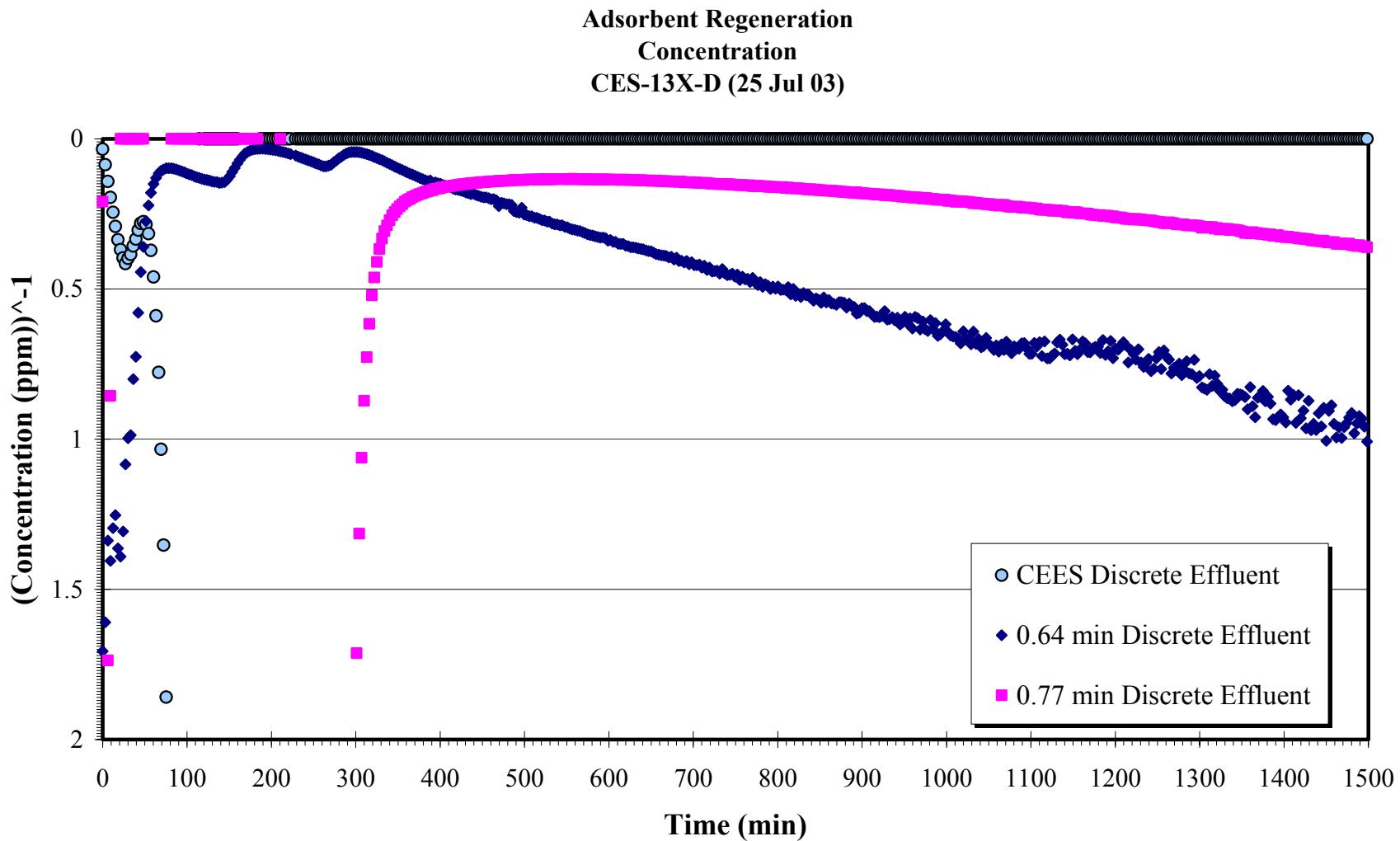
Results





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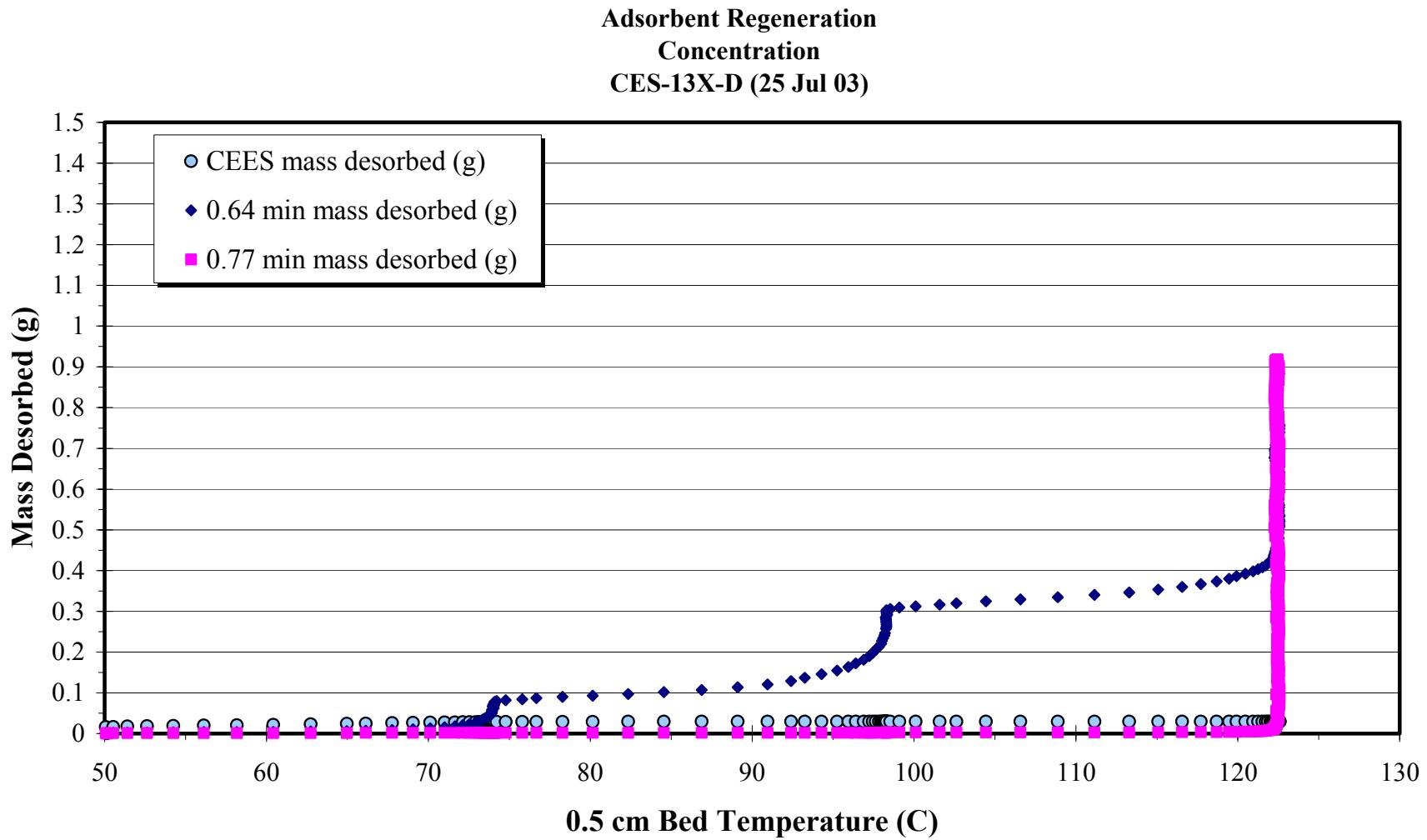
Results





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Results



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